# JOURNAL OF Chemical & **ENGINEERING** DATA

# Volumetric Properties for (Ionic Liquid + Methanol or Ethanol or 1-Propanol + Nitromethane) at 298.15 K and Atmospheric Pressure

Nirmala Deenadayalu,<sup>\*,†</sup> Indra Bahadur,<sup>†</sup> and Tadeusz Hofman<sup>‡</sup>

<sup>†</sup>Department of Chemistry, Durban University of Technology, P.O. Box 1334, Durban 4000, South Africa

\*Warsaw University of Technology, Faculty of Chemistry, Division of Physical Chemistry, ul. Nowakowskiego 3, 00-664 Warszawa, Poland

**ABSTRACT:** The densities of the ternary systems {1-butyl-3-methylimidazolium methyl sulfate ( $[BMIM]^+[MeSO_4]^-$ ) + methanol or ethanol or 1-propanol + nitromethane} were measured at the temperature 298.15 K, and the ternary excess molar volumes,  $V_{123}^{E}$ , were calculated. The  $V_{123}^{E}$  values are negative for all mole fractions of the ionic liquid (IL) and increase with increasing mole fraction of IL. The Cibulka equation was used to correlate the ternary excess molar volumes using the Redlich-Kister parameters for the binary systems obtained from the literature. There is a good correlation between the Cibulka equation and the experimental  $V_{123}^{\rm E}$  data.

## ■ INTRODUCTION

There is a lack of data on ternary excess molar volumes,  $V_{123}^{E}$ , for ionic liquid (IL) multicomponent systems.<sup>1-8</sup> Gómez et al.<sup>1</sup> determined  $V_{123}^{\rm E}$  for the IL system (ethanol + water + 1,3dimethylimidazolium methyl sulfate) at several temperatures. Deenadayalu et al.<sup>2</sup> used graph theory to correlate  $V_{123}^{E}$  for (1-ethyl-3-methylimidazolium diethylene glycol monomethyl ether sulfate + methanol + water) and calculated  $V_{123}^{E}$  for ([MOA]<sup>+</sup>- $[Tf_2N]^-$  + methanol or ethanol + methyl acetate or ethyl acetate)<sup>3,4</sup> at the temperatures (298.15, 303.15, and 313.15) K. González et al.<sup>6</sup> studied  $V_{123}^{E}$  for the (ethanol + water +1-butyl-

3-methylimidazolium methyl sulfate) ternary system at several temperatures. Andreatta et al.<sup>7,8</sup> studied  $V_{123}^{\rm E}$  for the systems [methyl acetate + methanol +1-octyl-3-methylimidazolium bis(trifluoromethylsulfonyl)imide] and [ethyl acetate + ethanol + 1-butyl-3methylimidazolium bis(trifluoromethylsulfonyl)imide] at the temperature 298.15 K and atmospheric pressure.

In this work, values of  $V_{123}^{\rm E}$  for the ternary IL systems  $([BMIM]^+[MeSO_4]^- + methanol or ethanol or 1- propanol +$ nitromethane) over the entire composition range were calculated from the experimental densities at the temperature 298.15 K and atmospheric pressure. The IL 1-butyl-3-methylimidazolium methyl sulfate ( $[BMIM]^+[MeSO_4]^-$ ) was used. This work is a continuation of our research group's work on thermodynamic properties of ILs.  $^{2-5,9-14}$ 

### EXPERIMENTAL SECTION

The solvents were purchased from Aldrich, Merck, and Fluka with mass fraction purity > 0.990 for methanol, ethanol, 1-propanol, and nitromethane and mass fraction purity > 0.970 for the IL. The IL, methanol, ethanol, 1-propanol, and nitromethane were used without any further purification. The water content in the IL was determined using a Karl Fischer coulometer (Metrohm model 797), and the mass fraction water content was found to be < 0.0024. The purity of the solvents was assessed by a comparison of the experimental density value with literature density values where available.<sup>9,15</sup>

The mass balance had a precision of 0.0001 g. The uncertainty in the mole fraction was estimated to be 0.0006.

The ternary mixtures were prepared to obtain a constant ratio of  $z = x_3/x_1$ , where  $x_1$  is the mole fraction of IL and  $x_3$  is the mole fraction of nitromethane, while varying the mole fraction of methanol or ethanol or 1-propanol  $(x_2)$ . The densities were measured with an Anton Paar DMA 38 vibrating U-tube densimeter. Ultrapure water supplied by SH Calibration Service GmbH Graz and dried air was used for the calibration of the densimeter at the temperature 298.15 K.<sup>9</sup> The temperature maintenance and control were regulated by a built-in thermostat controller with a temperature uncertainty of  $\pm$  0.01 K, and the densimeter was capable of measuring density to  $\pm$  0.0001  $g \cdot cm^{-3}$ . The uncertainty in the density for the ternary system was 0.002 g  $\cdot$  cm<sup>-3</sup>. The experimental uncertainty in  $V_{123}^E$  was  $\pm$ 0.1 cm<sup>3</sup> · mol<sup>-1</sup>. The literature and experimental densities ( $\rho$ ) are given in Table 1. The structure of the IL is given in Figure 1.

### RESULTS AND DISCUSSION

In Tables 2 to 4, the densities,  $\rho$ , and the excess molar volumes for the ternary systems,  $V_{123}^{E}$ , are given as functions of composition at the temperature 298.15 K. The  $V_{123}^{E}$  values were calculated from the experimental density values using the following equation:

$$V_{123}^{\rm E} = \frac{x_1 M_1 + x_2 M_2 + x_3 M_3}{\rho} - \frac{x_1 M_1}{\rho_1} - \frac{x_2 M_2}{\rho_2} - \frac{x_3 M_3}{\rho_3} \quad (1)$$

where  $x_1$ ,  $x_2$ , and  $x_3$  are the mole fractions,  $M_1$ ,  $M_2$ , and  $M_3$  the molecular masses, and  $\rho_1$ ,  $\rho_2$ , and  $\rho_3$  the densities of the pure components IL (1), methanol or ethanol or 1-propanol (2), and

Special Issue: John M. Prausnitz Festschrift

| Received:  | August 10, 2010   |
|------------|-------------------|
| Accepted:  | November 17, 2010 |
| Published: | January 26, 2011  |

1682

# Table 1. Literature and Experimental Densities of the Pure Compounds at T = 298.15 K

|  |               | ρ/g·                        | $ ho/g\cdot cm^{-3}$ |  |
|--|---------------|-----------------------------|----------------------|--|
| compound   | mass fraction | lit                         | exptl                |  |
| $[BMIM]^+[MeSO_4]^-$   | 0.970         | 1.20775 <sup><i>a</i></sup> | 1.2080               |  |
| methanol   | 0.998         | $0.78637^{b}$               | 0.7863               |  |
| ethanol  | 0.998         | 0.7855 <sup>b</sup>         | 0.7864               |  |
| 1-propanol   | 0.995         | $0.79960^{b}$               | 0.7976               |  |
| nitromethane   | 0.990         | 1.13117 <sup>a</sup>        | 1.1309               |  |
| <sup><i>a</i></sup> Data from ref 15. <sup><i>b</i></sup> Data from ref 9. |               |                             |                      |  |



Figure 1. 1-Butyl-3-methylimidazolium methyl sulfate,  $[BMIM]^+$ - $[MeSO_4]^-$ .

Table 2. Densities and Excess Molar Volumes for  $[BMIM]^+[MeSO_4]^-(1) + Methanol(2) + Nitromethane (3) at T = 298.15 K$ 

|        |                       | ρ                  | $V_{123}^{\mathrm{E}}$ |
|--------|-----------------------|--------------------|------------------------|
| $x_1$  | <i>x</i> <sub>2</sub> | g·cm <sup>-3</sup> | $cm^3 \cdot mol^{-1}$  |
| 0.0485 | 0.7471                | 0.959              | -0.9                   |
| 0.0903 | 0.5290                | 1.048              | -0.9                   |
| 0.1099 | 0.4269                | 1.081              | -0.9                   |
| 0.1452 | 0.2429                | 1.133              | -1.1                   |
| 0.1771 | 0.0765                | 1.164              | -0.8                   |
| 0.1332 | 0.6173                | 1.058              | -1.6                   |
| 0.1998 | 0.4256                | 1.115              | -1.4                   |
| 0.2390 | 0.3114                | 1.138              | -1.1                   |
| 0.2971 | 0.1467                | 1.168              | -0.8                   |
| 0.0603 | 0.8974                | 0.918              | -0.8                   |
| 0.1591 | 0.7290                | 1.042              | -1.5                   |
| 0.2494 | 0.5752                | 1.101              | -1.5                   |
| 0.3119 | 0.4692                | 1.129              | -1.3                   |
| 0.3705 | 0.3690                | 1.149              | -1.1                   |
| 0.4720 | 0.1965                | 1.175              | -0.6                   |
| 0.5271 | 0.1026                | 1.187              | -0.4                   |
| 0.3706 | 0.5428                | 1.129              | -1.3                   |
| 0.4692 | 0.4211                | 1.154              | -1.1                   |
| 0.5494 | 0.3222                | 1.170              | -0.8                   |
| 0.6151 | 0.2409                | 1.180              | -0.6                   |
| 0.7242 | 0.1053                | 1.194              | -0.2                   |
| 0.8468 | 0.1150                | 1.197              | -0.1                   |
| 0.7200 | 0.2475                | 1.184              | -0.4                   |

nitromethane (3), respectively, and  $\rho$  is the density of the mixture.

Binary excess molar volumes,  $V_{\rm m}^{\rm E}$ , for (IL + methanol),<sup>11</sup> (IL + ethanol),<sup>11</sup> (IL + 1-propanol),<sup>11</sup> (IL + nitromethane),<sup>15</sup> (methanol + nitromethane),<sup>16</sup> (ethanol + nitromethane),<sup>16</sup> and (1-propanol + nitromethane)<sup>17</sup> have been published in the literature. The binary  $V_{\rm m}^{\rm E}$  data are relatively small and do not

Table 3. Densities and Excess Molar Volumes for  $[BMIM]^+[MeSO_4]^-(1) + Ethanol(2) + Nitromethane (3)$  at T = 298.15 K

|        |                       | ρ                  | $V_{123}^{\mathrm{E}}$             |
|--------|-----------------------|--------------------|------------------------------------|
| $x_1$  | <i>x</i> <sub>2</sub> | g·cm <sup>-3</sup> | cm <sup>3</sup> ·mol <sup>-1</sup> |
| 0.0628 | 0.6726                | 0.954              | -0.8                               |
| 0.1076 | 0.4385                | 1.046              | -0.9                               |
| 0.1263 | 0.3412                | 1.080              | -1.0                               |
| 0.1568 | 0.1824                | 1.128              | -0.8                               |
| 0.1813 | 0.0545                | 1.162              | -0.7                               |
| 0.1640 | 0.5288                | 1.050              | -1.4                               |
| 0.2297 | 0.3403                | 1.109              | -1.1                               |
| 0.2898 | 0.1676                | 1.153              | -0.8                               |
| 0.3109 | 0.1070                | 1.166              | -0.7                               |
| 0.0829 | 0.8588                | 0.914              | -0.8                               |
| 0.2045 | 0.6517                | 1.035              | -1.3                               |
| 0.3024 | 0.4850                | 1.096              | -1.3                               |
| 0.3638 | 0.3807                | 1.125              | -1.1                               |
| 0.4175 | 0.2891                | 1.147              | -0.9                               |
| 0.5020 | 0.1454                | 1.175              | -0.6                               |
| 0.2942 | 0.6370                | 1.064              | -1.3                               |
| 0.4439 | 0.4523                | 1.125              | -1.2                               |
| 0.5383 | 0.3359                | 1.151              | -0.9                               |
| 0.6637 | 0.1808                | 1.178              | -0.4                               |
| 0.7482 | 0.0757                | 1.194              | -0.2                               |
| 0.8775 | 0.0829                | 1.197              | -0.1                               |
| 0.7787 | 0.1862                | 1.182              | -0.2                               |
| 0.6796 | 0.2898                | 1.166              | -0.5                               |

vary greatly with temperature. The Redlich–Kister equation<sup>18</sup> was fitted to the binary literature data to obtain the Redlich– Kister parameters at the temperature 298.15 K. The binary parameters are given in Table 5. The Redlich–Kister equation is given below:

$$V_{\rm m}^{\rm E} = x_1 x_2 \sum_{i=0}^{N} A_i (x_1 - x_2)^i$$
 (2)

The ternary excess molar volumes were correlated using the Cibulka equation,<sup>19</sup> which is given below:

$$V_{123}^{\rm E} = \sum_{i,j=1,2;1,3;2,3} V_{ij}^{\rm E}(x_i, x_j) - x_1 x_2 x_3 (b_0 - b_1 x_1 - b_2 x_2)$$
(3)

The Cibulka equation contains three parameters  $(b_0, b_1, \text{ and } b_2)$  corrected over the three binary contributions. The values of  $b_0$ ,  $b_1$ , and  $b_2$  were adjusted to the experimental ternary excess molar volumes and detailed in an earlier paper.<sup>4</sup> The smoothing coefficients and the relative mean standard deviation (rmsd) values,  $\sigma$ , are given in Table 6. Ternary graphs obtained using the Cibulka equation parameters are given in Figures 2 to 4.

For the binary systems (methanol or ethanol or 1-propanol + nitromethane) at the temperature 298.15 K, at all mole fractions of alkanol,  $V_m^E$  is negative because of the geometrical fitting of the nitromethane into the remaining alkanol structure.<sup>11</sup> The  $V_m^E$  values for (1-propanol + nitromethane) are greater than those

Table 4. Densities and Excess Molar Volumes for  $[BMIM]^+[MeSO_4]^-(1) + 1$ -Propanol (2) + Nitromethane (3) at T = 298.15 K

|        |                       | ρ                  | $V_{123}^{\rm E}$     |
|--------|-----------------------|--------------------|-----------------------|
| $x_1$  | <i>x</i> <sub>2</sub> | g·cm <sup>-3</sup> | $cm^3 \cdot mol^{-1}$ |
| 0.0979 | 0.4893                | 1.004              | -0.5                  |
| 0.1372 | 0.2842                | 1.079              | -0.6                  |
| 0.1637 | 0.1460                | 1.126              | -0.5                  |
| 0.1836 | 0.0423                | 1.160              | -0.5                  |
| 0.0745 | 0.6116                | 0.957              | -0.4                  |
| 0.1199 | 0.3745                | 1.046              | -0.6                  |
| 0.0539 | 0.7187                | 0.915              | -0.4                  |
| 0.0350 | 0.8172                | 0.875              | -0.2                  |
| 0.1871 | 0.4625                | 1.049              | -0.9                  |
| 0.2495 | 0.2834                | 1.108              | -0.8                  |
| 0.2803 | 0.1947                | 1.134              | -0.6                  |
| 0.3188 | 0.0841                | 1.166              | -0.5                  |
| 0.1454 | 0.5823                | 1.005              | -1.0                  |
| 0.1639 | 0.7208                | 0.977              | -0.8                  |
| 0.1037 | 0.8234                | 0.921              | -0.6                  |
| 0.2412 | 0.5892                | 1.036              | -0.9                  |
| 0.3410 | 0.4193                | 1.095              | -0.8                  |
| 0.3993 | 0.3203                | 1.124              | -0.7                  |
| 0.4477 | 0.2377                | 1.146              | -0.6                  |
| 0.5197 | 0.1153                | 1.175              | -0.4                  |
| 0.3456 | 0.5736                | 1.064              | -0.8                  |
| 0.4964 | 0.3876                | 1.124              | -0.7                  |
| 0.5841 | 0.2794                | 1.151              | -0.6                  |
| 0.6930 | 0.1447                | 1.179              | -0.4                  |
| 0.8948 | 0.0648                | 1.197              | -0.0                  |
| 0.8141 | 0.1492                | 1.183              | -0.1                  |
| 0.7289 | 0.2382                | 1.167              | -0.3                  |

for the (ethanol + nitromethane) > (methanol + nitromethane) systems because of the increase in alcohol chain length.<sup>11</sup>

For the binary systems (IL + methanol or ethanol or 1propanol) at T = 298.15 K, the  $V_m^E$  values are negative for all mole fractions of the IL because of the more efficient packing and/or attractive interaction that occurs when the IL and the alkanols are mixed.<sup>11</sup> The excess molar volumes increase in the order (IL + methanol) < (IL + ethanol) < (IL + 1-propanol) because of the increase in alcohol chain length.<sup>11</sup>

For the system (IL + nitromethane),  $V_m^E$  is negative at T = 298.15 K for all mole fractions of the IL as a result of packing effects.<sup>15</sup>

The binary  $V_{\rm m}^{\rm E}$  data for (methanol + nitromethane),<sup>16</sup> (IL + methanol),<sup>11</sup> and (IL + nitromethane)<sup>15</sup> at the temperature 298.15 K are all negative because of the geometrical fitting of the nitromethane molecules into the methanol structure for the first binary system and a more efficient packing and/or attractive interaction between the IL and the methanol or nitromethane molecules for the latter two binary systems. The negative values of  $V_{123}^{\rm E}$  for (IL + methanol + nitromethane) show that the ion—dipole interactions and packing effects among methanol, nitromethane, and the IL dominate over the dissociation of the intermolecular hydrogen bonds in methanol and nitromethane.<sup>3</sup> At high mole fractions of methanol or IL and low mole fractions of

| Table 5.  | Redlich-   | Kister I | Parameters | for th | e Seven | Binary |
|-----------|------------|----------|------------|--------|---------|--------|
| Systems a | at T = 298 | .15 K    |            |        |         |        |

|  |       |                         |                 |                        | σ                     |
|--|-------|-------------------------|-----------------|------------------------|-----------------------|
| $A_0$  | $A_1$ | $A_2$                   | $A_3$           | $A_4$                  | $cm^3 \cdot mol^{-1}$ |
|  | [I    | 3MIM]+[Me               | $[SO_4]^- + N$  | [ethanol <sup>a</sup>  |                       |
| 4.13   | -2.63 | 0.16                    | _               | _                      | 0.01                  |
|  | [     | BMIM] <sup>+</sup> [M   | $[eSO_4]^- + I$ | Ethanol <sup>a</sup>   |                       |
| 2.50   | -0.93 | -0.08                   | _               | _                      | 0.009                 |
|  | [B    | MIM] <sup>+</sup> [Me   | $SO_4]^- + 1-1$ | Propanol <sup>a</sup>  |                       |
| 0.95   | -0.19 | _                       | _               | _                      | 0.009                 |
|  | [BN   | IIM] <sup>+</sup> [MeSo | $O_4]^- + Nitr$ | romethane <sup>b</sup> |                       |
| -1.92  | 1.34  | -0.47                   | 1.58            | -1.86                  | 0.01                  |
| Methanol + Nitromethane <sup>c</sup>   |       |                         |                 |                        |                       |
| -0.70  | -0.40 | -0.29                   | _               | _                      | 0.003                 |
| $E than ol + N itromethan e^{c}$   |       |                         |                 |                        |                       |
| 0.05   | -0.57 | -0.35                   | -0.59           | -                      | 0.005                 |
| $1	ext{-Propanol} + \operatorname{Nitromethane}^d$   |       |                         |                 |                        |                       |
| 0.94   | -0.26 | 0.15                    | -0.41           | _                      | 0.001                 |
| Experimental data from ref 11. <sup>b</sup> Experimental data from ref 15.<br>Experimental data from ref 16. <sup>d</sup> Experimental data from ref 17. |       |                         |                 |                        |                       |

Table 6. Smoothing Coefficients  $b_n$  and Relative Mean Standard Deviations  $\sigma$  for the Cibulka Equation at T = 298.15 K

|  |                            |                       | σ                     |  |
|--|----------------------------|-----------------------|-----------------------|--|
| $b_0$  | $b_1$                      | $b_2$                 | $cm^3 \cdot mol^{-1}$ |  |
| [BMIM  | $]^{+}[MeSO_{4}]^{-}(1) +$ | - Methanol (3) + Ni   | tromethane (3)        |  |
| 35.60  | -52.47                     | - 185.50              | 0.74                  |  |
| [BMIN  | $[MeSO_4]^-(1)$            | + Ethanol $(2)$ + Nit | romethane (3)         |  |
| 14.68  | -29.73                     | - 133.66              | 0.74                  |  |
| $[BMIM]^{+}[MeSO_{4}]^{-}(1) + 1$ -Propanol (2) + Nitromethane (3) |                            |                       |                       |  |
| 5.86   | -9.83                      | - 86.03               | 0.31                  |  |

nitromethane, the  $V_{123}^{\text{E}}$  values are positive, indicating that as the nitromethane mole fraction increases, the minimum of the  $V_{123}^{\text{E}}$  value shifts from the binary (IL + nitromethane) system into the middle of the ternary concentration.

The binary  $V_{\rm m}^{\rm E}$  data for (ethanol + nitromethane)<sup>16</sup> at the temperature 298.15 K exhibit both positive and negative values because of the breakup of the ethanol structure and geometrical fitting of the nitromethane into the ethanol structure, respectively.<sup>16</sup> The binary  $V_{\rm m}^{\rm E}$  data for (IL + ethanol) at the temperature 298.15 K is negative at all mole fractions of the IL. The ternary  $V_{123}^{\rm E}$  values for (IL + ethanol + nitromethane) are similar to those for (IL + methanol + nitromethane).

The binary  $V_{\rm m}^{\rm E}$  data for (IL + 1-propanol) at the temperature 298.15 K are negative for all mole fractions of IL as a result of the same effects that occur in the (IL + methanol) binary system. For the binary system of (1-propanol + nitromethane) at the temperature 298.15 K and at all mole fractions of 1-propanol,  $V_{\rm m}^{\rm E}$  is positive because of the rupture of hydrogen bonds and dispersive interactions between unlike molecules.<sup>17</sup> The binary excess



**Figure 2.** Graph of the excess molar volume,  $V_{123}^{E}$ , of the ternary mixture  $[BMIM]^{+}[MeSO_{4}]^{-}(1)$  + methanol (2) + nitromethane (3) at 298.15 K. Solid lines were calculated with the Cibulka equation using the values of the parameters fitted to the binary and ternary data.



**Figure 3.** Graph of the excess molar volume,  $V_{123}^E$ , of the ternary mixture  $[BMIM]^+[MeSO_4]^-(1)$  + ethanol (2) + nitromethane (3) at T = 298.15 K. Solid lines were calculated with the Cibulka equation using the values of the parameters fitted to the binary and ternary data.



**Figure 4.** Graph of the excess molar volume,  $V_{123}^{E}$ , of the ternary mixture  $[BMIM]^{+}[MeSO_{4}]^{-}(1) + 1$ -propanol (2) + nitromethane (3) at T = 298.15 K. Solid lines were calculated with the Cibulka equation using the values of the parameters fitted to the binary and ternary data.

molar volumes increase in the order (methanol + nitromethane) < (ethanol + nitromethane) < (1-propanol + nitromethane) systems because of the increase in alcohol chain length, which causes a decrease in attractive interaction between the two types of molecules. The negative values of  $V_{123}^{E}$  for (IL + 1-propanol + nitromethane) are due to the same effects has explained previously for the (IL + methanol or ethanol + nitromethane) ternary systems.  $V_{123}^{E}$  increases for the ternary systems in the order (IL + methanol + nitromethane) < (IL + ethanol + nitromethane) < (IL + ethanol + nitromethane).

The Cibulka equation correlations indicate that the ternary contribution (three-body effect) is dominant. The molecules of IL, methanol or ethanol or 1-propanol, and nitromethane are engaged in specific interactions, and the ability of methanol or ethanol or 1-propanol to form hydrogen bonds with the IL is increased by the presence of the nitromethane molecules.

### CONCLUSION

In this paper, the densities and  $V_{123}^{E}$  have been reported for the systems (IL + methanol or ethanol or 1-propanol + nitromethane) at T = 298.15 K. The  $V_{123}^{E}$  values are negative for all compositions of the IL and show that the ion—dipole interactions as well as the packing effects among the alcohol, nitromethane, and the IL dominate over the dissociation of intermolecular hydrogen bonds in the alcohol and nitromethane. The molecules of IL, methanol or ethanol or 1-propanol, and nitromethane are engaged in specific interactions, and the ability of methanol or ethanol or 1-propanol to form hydrogen bonds with the IL is increased by the presence of nitromethane molecules. The Cibulka equation was used to correlate the ternary data and indicated that the ternary contribution to  $V_{123}^{E}$  is dominant.

## AUTHOR INFORMATION

#### **Corresponding Author**

\*E-mail: NirmalaD@dut.ac.za. Telephone: +27 31 3732781. Fax: +27 31 2022671.

### REFERENCES

(1) Gómez, E.; González, B.; Calvar, N.; Domínguez, Á. Excess molar properties of ternary system (ethanol + water + 1, 3-dimethylimidazolium methylsulphate) and its binary mixtures at several temperatures. J. Chem. Thermodyn. 2008, 40, 1208–1216.

(2) Deenadayalu, N.; Kumar, S.; Bhujrajh, P. Liquid densities and excess molar volumes for (ionic liquids + methanol + water) ternary system at atmospheric pressure and at various temperatures. *J. Chem. Thermodyn.* **2007**, *39*, 1318–1324.

(3) Deenadayalu, N.; Bhujrajh, P. Density, Speed of Sound, and Derived Thermodynamic Properties of Ionic Liquids  $[EMIM]^+[BETI]^-$  or  $([EMIM]^+[CH_3(OCH_2CH_2)_2OSO_3]^- +$  Methanol or + Acetone) at T = (298.15 or 303.15 or 313.15) K. *J. Chem. Eng. Data* **2008**, *53*, 1098–1102.

(4) Deenadayalu, N.; Bahadur, I.; Hofman, T. Ternary Excess Molar Volumes of {Methyltrioctylammonium Bis[(trifluoromethyl)sulfonyl]imide + Methanol + Methyl Acetate or Ethyl Acetate} Systems at (298.15, 303.15, and 313.15) K. J. Chem. Eng. Data **2010**, 55, 2636–2642.

(5) Deenadayalu, N.; Bahadur, I.; Hofman, T. Ternary excess molar volumes of {methyltrioctylammonium bis[(trifluoromethyl)sulphonyl]imide + methanol + methyl acetate or ethyl acetate} systems at (298.15, 303.15, and 313.15) K. J. Chem. Thermodyn. **2010**, *42*, 726–733.

(6) González, B.; Calvar, N.; Gómez, E.; Domínguez, Á. Physical properties of the ternary system (ethanol + water + 1-butyl-3-methylimidazolium methylsulphate) and its binary mixtures at several temperatures. J. Chem. Thermodyn. 2008, 40, 1274–1281. (7) Andreatta, A. E.; Arce, A.; Rodil, E.; Soto, A. Physical and excess properties of (methyl acetate + methanol + 1-octyl-3-methylimidazolium bis(trifluoromethylsulfonyl)imide) and its binary mixtures at T = 298.15 K and atmospheric pressure. *J. Chem. Thermodyn.* 2009, 41, 1317–1323.

(8) Andreatta, A. E.; Arce, A.; Rodil, E.; Soto, A. Physico-chemical Properties of Binary and Ternary mixtures of (Ethyl acetate + Ethanol + 1-Butyl-3-methylimidazolium bis(trifluoromethylsulfonyl)imide) at T = 298.15 K and Atmospheric Pressure. *J. Solution Chem.* **2010**, *39*, 371–383.

(9) Sibiya, P. N.; Deenadayalu, N. Excess molar volumes and isentropic compressibility of binary systems {trioctylmethylammonium bis-(trifluoromethysulfonyl)imide + methanol or ethanol or 1-propanol} at different temperatures. *J. Chem. Thermodyn.* **2008**, *40*, 1041–1045.

(10) Deenadayalu, N.; Sen, S.; Sibiya, P. N. Application of the PFV EoS correlation to excess molar volumes of (1-ethyl-3-methylimidazolium ethylsulfate + alkanols) at different temperatures. *J. Chem. Thermodyn.* **2009**, *41*, 538–548.

(11) Sibiya, P. N.; Deenadayalu, N. Excess Molar Volumes and Partial Molar Volumes of Binary Systems (Ionic Liquid + Methanol or Ethanol or 1-Propanol) at T = (298.15, 303.15 and 313.15) K. S. Afr. J. Chem. 2009, 62, 20–25.

(12) Bhujrajh, P.; Deenadayalu, N. Liquid Densities and Excess Molar Volumes for Binary Systems (Ionic Liquids + Methanol or Water) at 298.15, 303.15 and 313.15 K, and at Atmospheric Pressure. *J. Solution Chem.* **2007**, *36*, 631–642.

(13) Deenadayalu, N.; Ngcongo, K. C.; Letcher, T. M.; Ramjugernath, D. Liquid–Liquid Equilibria for Ternary Mixtures (an Ionic Liquid + Benzene + Heptane or Hexadecane) at *T* = 298.2 K and Atmospheric Pressure. *J. Chem. Eng. Data* **2006**, *51*, 988–991.

(14) Deenadayalu, N.; Thango, S. H.; Letcher, T. M.; Ramjugernath, D. Measurement of activity coefficients at infinite dilution using polar and non-polar solutes in the ionic liquid 1-methyl-3-octylimidazolium diethyleneglycolmonomethylethersulfate at T = (288.15, 298.15, and 313.15) K. J. Chem. Thermodyn. **2006**, *38*, 542–546.

(15) Iglesias-Otero, M. A.; Troncoso, J.; Carballo, E.; Romani, L. Density and refractive index in mixtures of ionic liquids and organic solvents: Correlations and predictions. *J. Chem. Thermodyn.* **2008**, *40*, 949–956.

(16) Nakanishi, K.; Shirai, H. Studies on Associated Solutions. I. Excess Volume of Binary Systems of Alcohols with Various Organic Liquids. *Bull. Chem. Soc. Jpn.* **1970**, *43*, 1634–1642.

(17) Cerdeirina, C. A.; Tover, C. A.; Troncoso, J.; Carballo, E.; Romani, L. Excess volumes and excess heat capacities of nitromethane + (1-propanol or 2-propanol). *Fluid Phase Equilib.* **1999**, *157*, 93–102.

(18) Redlich, O.; Kister, A. T. Algebraic representation of thermodynamic properties and classification of solutions. *Ind. Eng. Chem.* **1948**, *40*, 345–348.

(19) Cibulka, I. Estimation of excess volume and density of ternary liquid mixtures of nonelectrolytes from binary data. *Coll. Czech. Commun.* **1982**, *47*, 1414–1419.